

# **Adsorption of radioactives nobles gases in microporous materials**

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# Radioactive gases in nature

${}^3\text{H}$ (12.3 y)	Cosmogenic Anthropogenic
${}^{36}\text{Cl}$ ( $3.10^5$ y)	Comogenic
${}^{37}\text{Ar}$ (35 d)	Cosmogenic
${}^{39}\text{Ar}$ (269 y)	Cosmogenic
${}^{42}\text{Ar}$ (42 y)	Cosmogenic
${}^{81}\text{Kr}$ ( $2.310^5$ y)	Cosmogenic
${}^{85}\text{Kr}$ (10.8 y)	Anthropogenic
${}^{88}\text{Kr}$ (42.3 d)	Anthropogenic
${}^{129}\text{I}$ ( $1.6.10^7$ y)	Anthropogenic
${}^{133}\text{Xe}$ (5.28 y)	Anthropogenic
${}^{135}\text{Xe}$ (127.7 d)	Anthropogenic
${}^{222}\text{Rn}$ (3.8 d)	Natural decay chains ( ${}^{235}\text{U}$ , ${}^{238}\text{U}$ , ${}^{232}\text{Th}$ )

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**Noble gases**

# Radioactive gases in nature

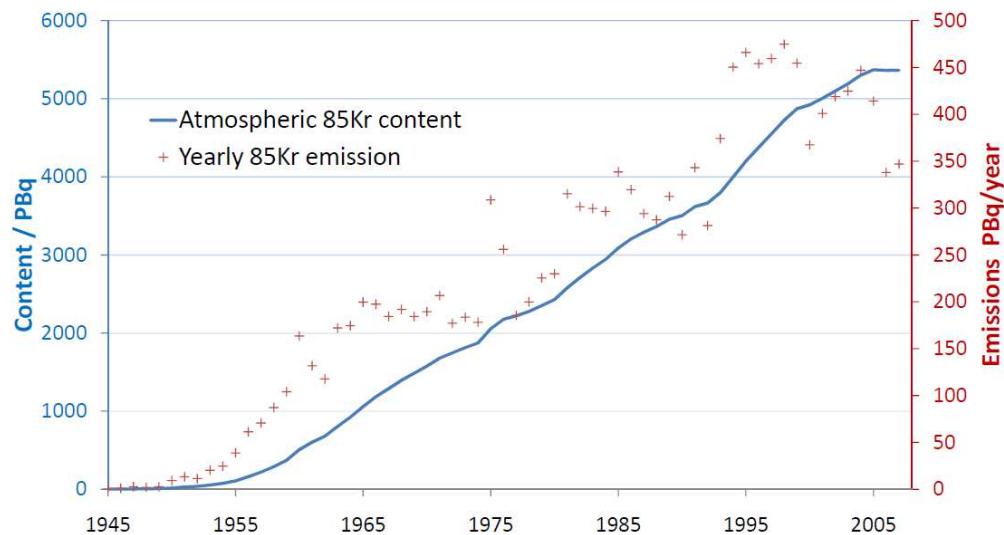
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Noble gases

# Some noble gases concentration in air

□  $^{39}\text{Ar}$   $\Rightarrow 11 \text{ mBq/m}^3$

□  $^{85}\text{Kr}$   $\Rightarrow 1 \text{ Bq/m}^3$



Increase  $0.025 \text{ Bq/m}^3/\text{y}$

□  $^{222}\text{Rn}$   $\Rightarrow 10 - 100 \text{ Bq/m}^3$

# Capture of noble gases

A periodic table where the noble gases (He, Ne, Ar, Kr, Xe, Rn) are highlighted in red. The entire group is enclosed in a red rectangular border.

IA	IIA	noble gases																		0
1	H																			He
2	Li	Be																		Ne
3	Na	Mg	IIIIB	IVB	VB	VIIB	VIIIB	—	VII	—	IB	IIIB	IIIA	IVA	V A	VIA	VII A			O
4	K	Ca	Sc	Ti	V	Cr	Mn	Fe	Co	Ni	Cu	Zn	Ga	Ge	As	Se	Br			F
5	Rb	Sr	Y	Zr	Nb	Mo	Tc	Ru	Rh	Pd	Ag	Cd	In	Sn	Sb	Te	I			Cl
6	Cs	Ba	*La	Hf	Ta	W	Re	Os	Ir	Pt	Au	Hg	Tl	Pb	Bi	Po	At			Ar
7	Fr	Ra	+Ac	Rf	Ha	Sg	Ns	Hs	Mt	110	111	112	113							Rn

Table 1. Experimentally identified noble-gas hydride molecules by the year 2009.

		HXeH
		HXeI
		HXeBr
	HKrCl	HXeCl
HArF	HKrF	
	HKrCN	HXeCN
		HXeNC
		HXeOH
		HXeO
		HXeOXeH
		HXeSH
		HXeNCO
	HKrCCH	HXeCCH
	HKrCCCN	HXeCCCN
		HXeCCXeH
		HXeCC
	HKrCCCCH	HXeCCCCH

## Noble gases

Full outer shell ( 8 e<sup>-</sup>)  
=> no valence electrons  
=> very small reactivity

## Nevertheless

Possible compounds for heavier noble elements  
Kr, Xe

Rn must interact with matter better than Xe  
However radon is a pure radioactive short period gas  
=> poor knowledge of chemical properties

Chemistry of noble gases is possible  
but very poor

Very difficult capture by chemisorption

# Radioactivity from noble gases is an important background for many low-activity low-count experiments

- Krypton ( $^{85}\text{Kr}$ )

Beta emitter:  $E_{\max} = 687 \text{ keV}$ ,  $\gamma$  of 514 keV @ 0.43 %

- Argon ( $^{39}\text{Ar}$ )

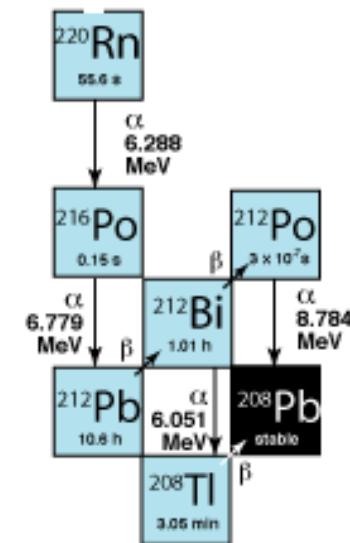
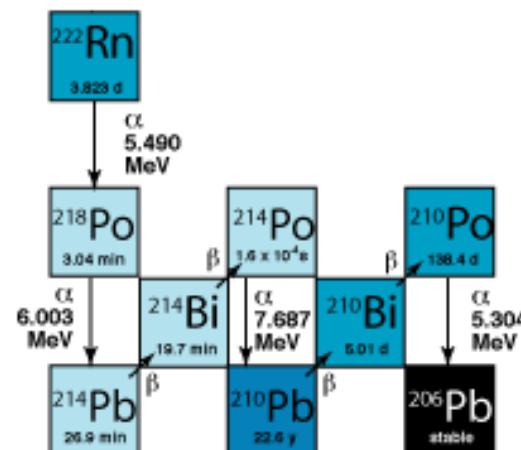
Beta emitter:  $E_{\max} = 565 \text{ keV}$ , no gamma!

- Radon ( $^{220}\text{Rn}$ ,  $^{222}\text{Rn}$ )

Alpha emitter up to 8.8 MeV

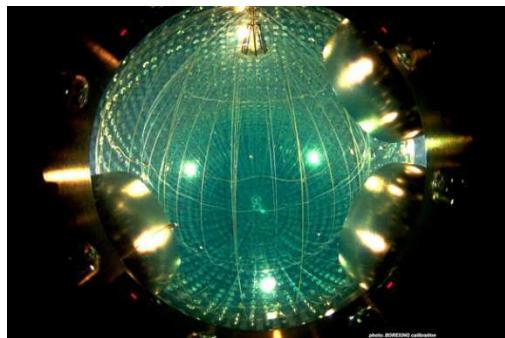
Beta emitter up to 5 MeV

Gamma up to 2.6 MeV



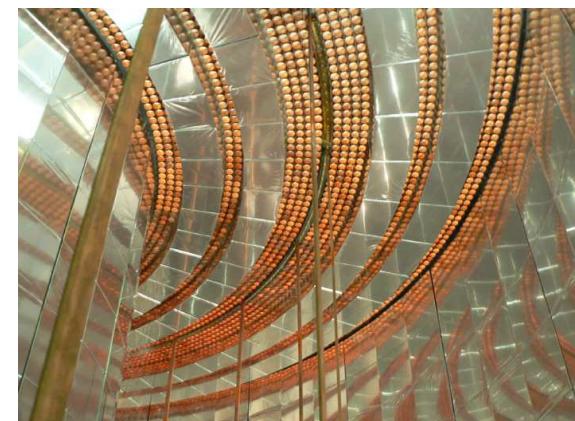
# Radioactivity from noble gases is an important background for many low-activity low-count experiments

Borexino Solar  
Neutrino experiment



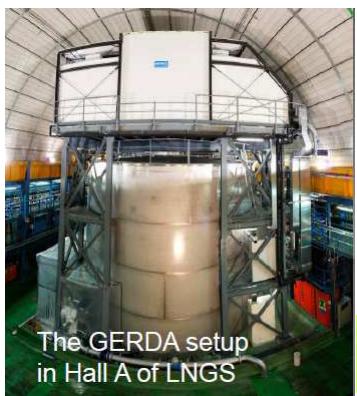
$^{85}\text{Kr} \rightarrow < 0.2 \mu\text{Bq}/\text{m}^3$   
 $^{39}\text{Ar} \rightarrow < 0.5 \mu\text{Bq}/\text{m}^3$

SuperNEMO  
 $\beta\beta$  experiment



$^{222}\text{Rn} \rightarrow < 150 \mu\text{Bq}/\text{m}^3$  ( $< 100 \text{ atoms / m}^3$ )

Gerda  
 $\beta\beta$  experiment



The GERDA setup  
in Hall A of LNGS

$^{85}\text{Kr} \rightarrow < 2 \text{ ppt}$

$^{42}\text{Ar} \rightarrow < 40 \mu\text{Bq/L}$

LUX dark matter experiment

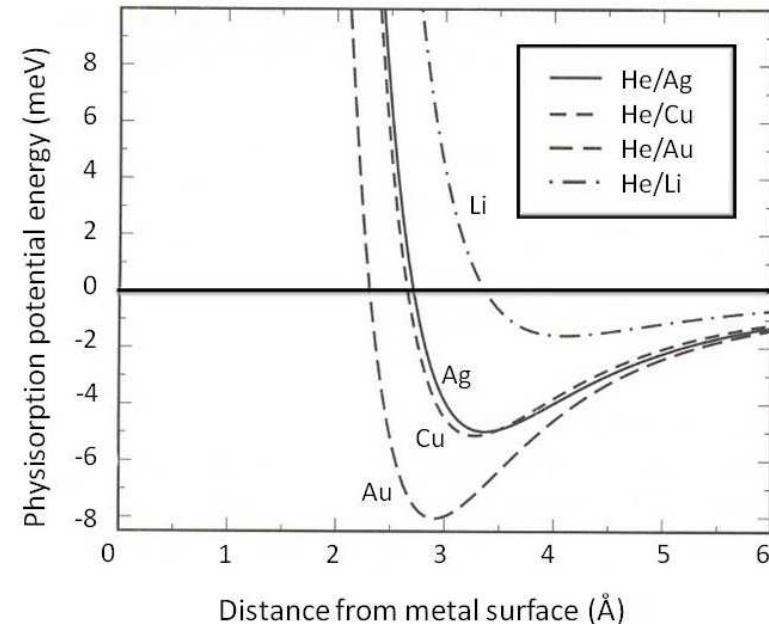
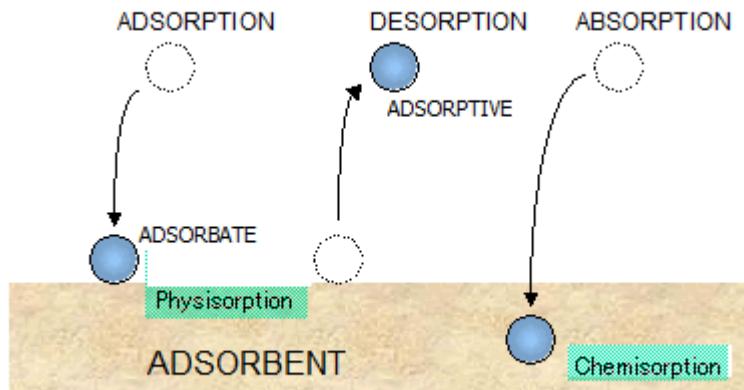


# Nobel gases adsorption

Nobel gas => capture mainly by physisorption (adsorption)

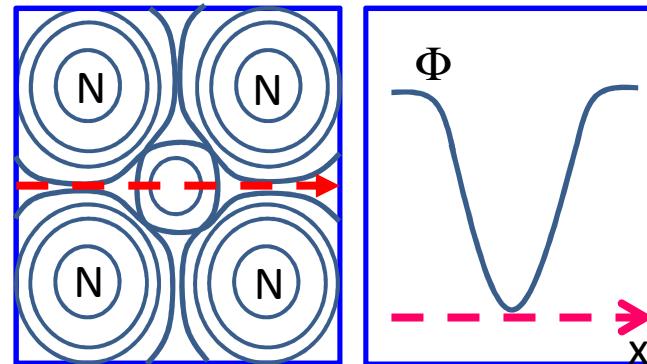
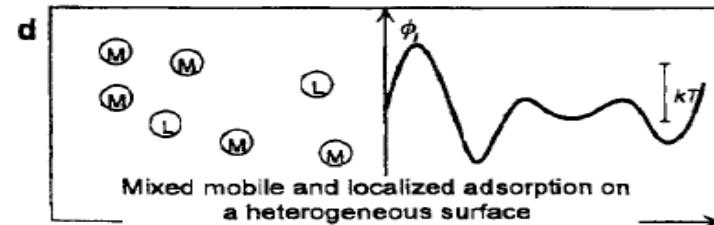
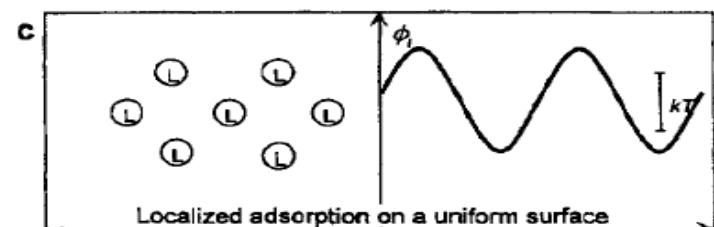
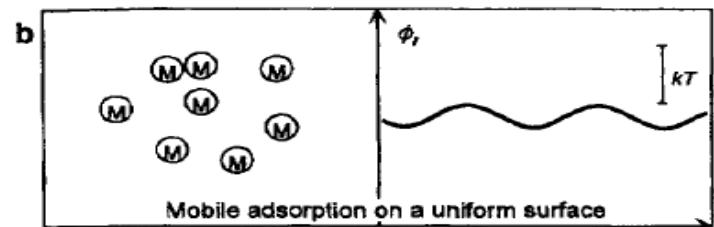
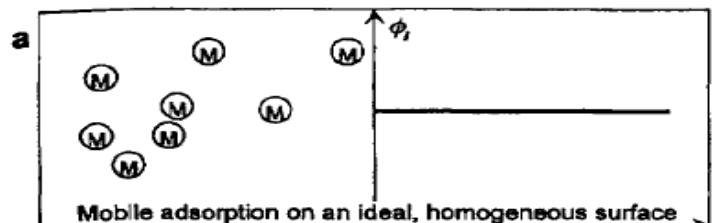
→ Weak Van der Waals

Capture on surface



Equilibrium between Adsorption and Desorption

# Transport of adsorbed molecules



If  $\Phi$  is much smaller than thermal energy ,  $kT$ , the molecules are regarded as “mobile”.

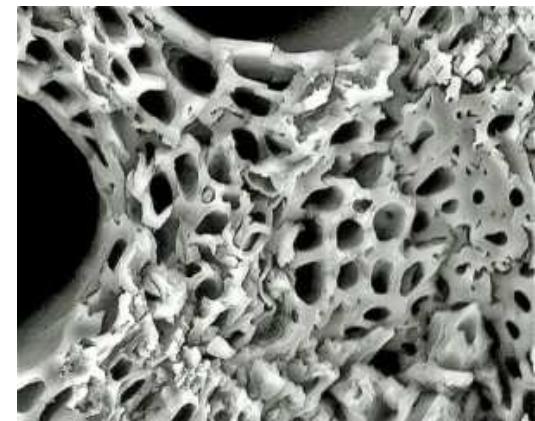
If  $\Phi$  is much larger than  $kT$ , the molecules are “localized”.

## To increase the capture capacity we need :

- **increase the surface area => high porosity**
- **reduced the temperature**

Typical porosity of active charcoals :

sample	A	B	C
N2 77K			
BET surface area ( $\text{m}^2/\text{g}$ )	1740	1077	1355
BET avg pore diameter ( $\text{\AA}$ )	21.71	19.95	24.98
HK total pore volume ( $\text{cm}^3/\text{g}$ ; $<200 \text{ \AA}$ )	0.944	0.537	0.846
HK micropore volume ( $\text{cm}^3/\text{g}$ ; $<20 \text{ \AA}$ )	0.768	0.511	0.544
HK narrow micropore volume ( $\text{cm}^3/\text{g}$ ; $<6 \text{ \AA}$ )	0.282	0.281	0.125
HK broad micropore volume ( $\text{cm}^3/\text{g}$ ; $6\text{-}20 \text{ \AA}$ )	0.486	0.229	0.419
Hg porosimetry			
total pore volume ( $\text{cm}^3/\text{g}$ ; $66\text{-}10^5 \text{ \AA}$ )	0.469	0.221	0.751
mesopore volume ( $\text{cm}^3/\text{g}$ ; $66\text{-}500 \text{ \AA}$ )	0.101	0.054	0.266
macropore volume ( $\text{cm}^3/\text{g}$ ; $500\text{-}10^5 \text{ \AA}$ )	0.368	0.167	0.485



Enormous surface area  
of active charcoal

The effective surface area is distributed between different porous size

# Pore size and atomic radius

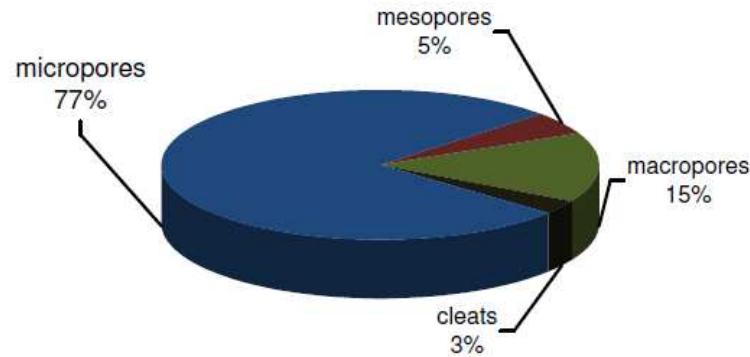
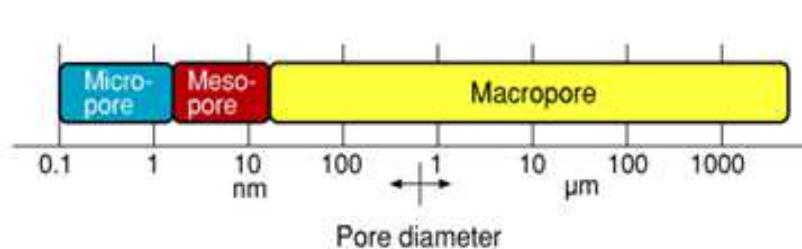
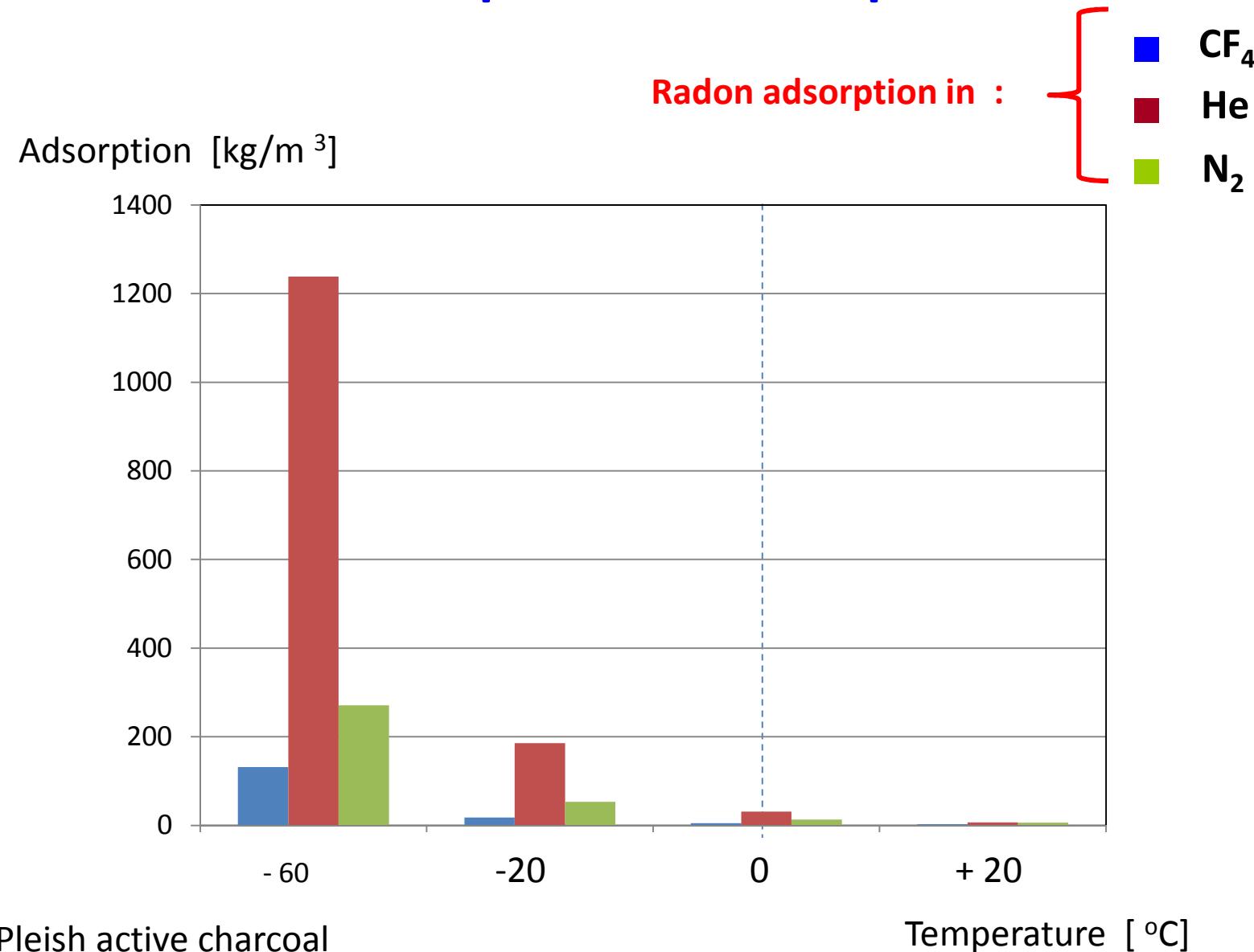


Figure 3.1: Example Pore Size Distribution in Coal (Mardon 2008)

	Gas	van der Waals	Covalent (single bond)	Covalent (triple bond)	Atomic radius
			nanometer		
	He	0.14	0.032	-	
	N	0.155	0.075	0.054	
	Ar	0.188	0.097	0.096	
	Kr	0.202	0.110	0.108	
	Xe	0.216	0.130	0.122	
	Rn	0.220	0.145	0.133	

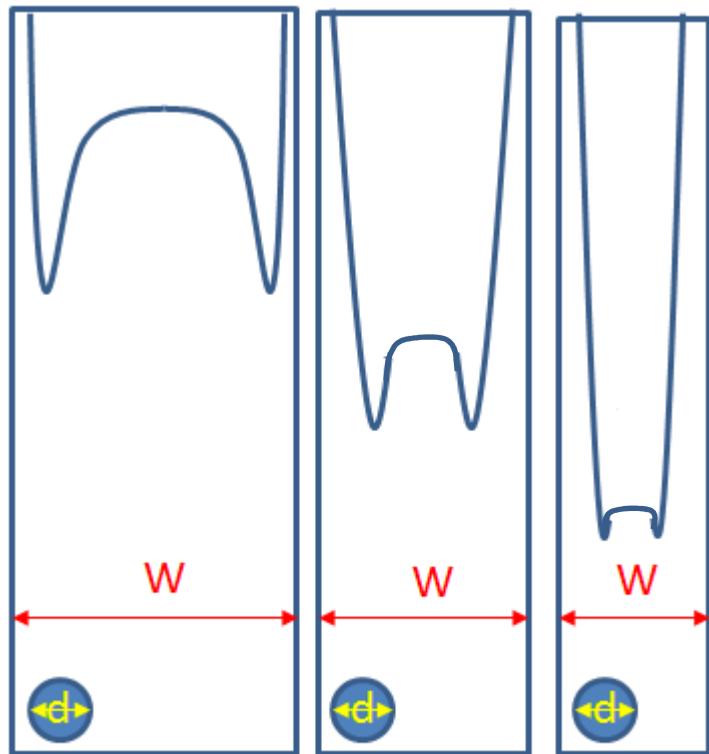
Competition between carrier gas and radon

# Adsorption competition



# Enhancement of the energy of adsorption in slit shaped pores of various widths

Van der Waals potential well in a narrow porous

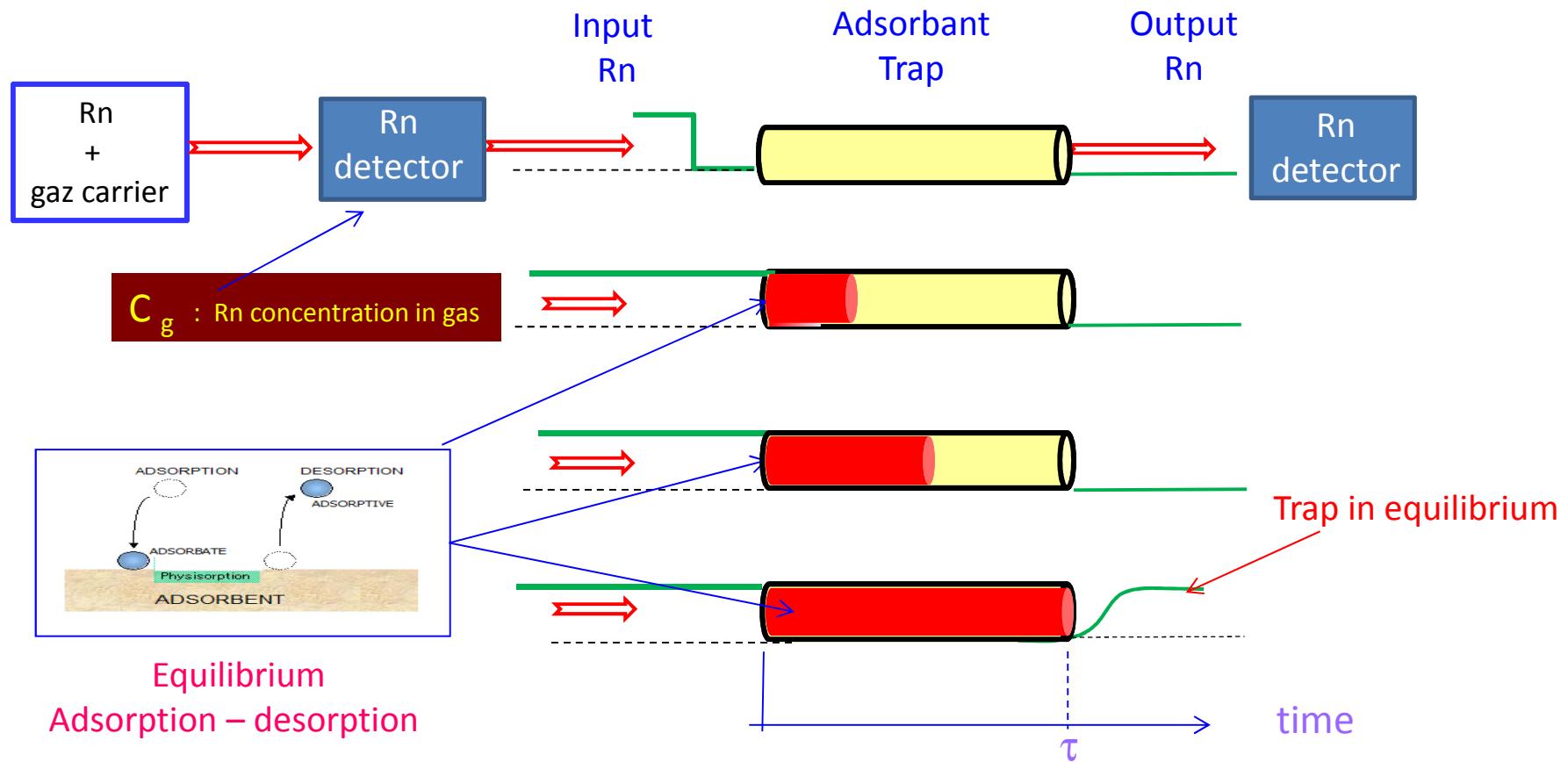


The size and the shape of the pores  
has to be optimum

# Radon capture measurements at CPPM

Characterization of radon adsorption on microporous materials

# Radon capture measurement by dynamic technique

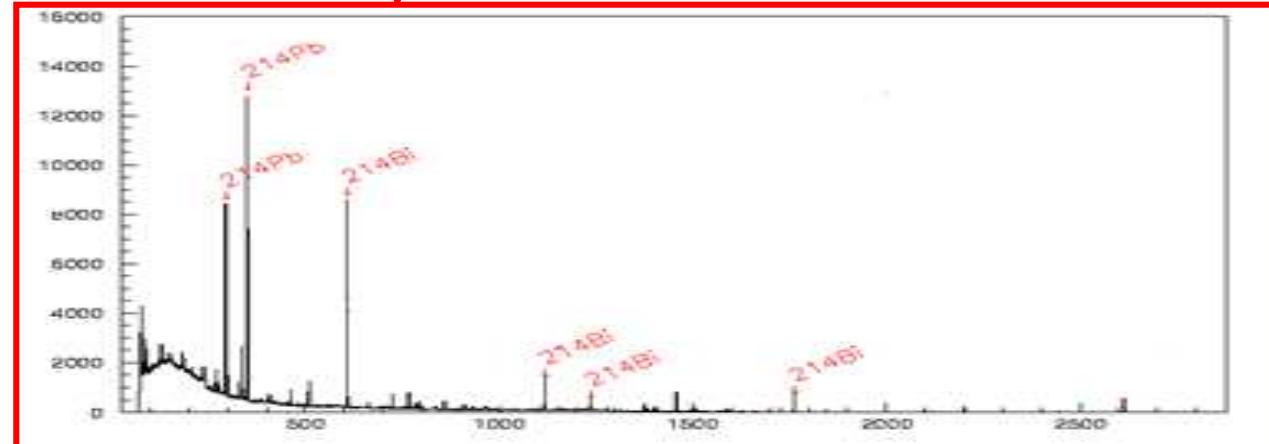


# Radon capture measurement by dynamic technique



$C_m$  : Rn concentration in the trap

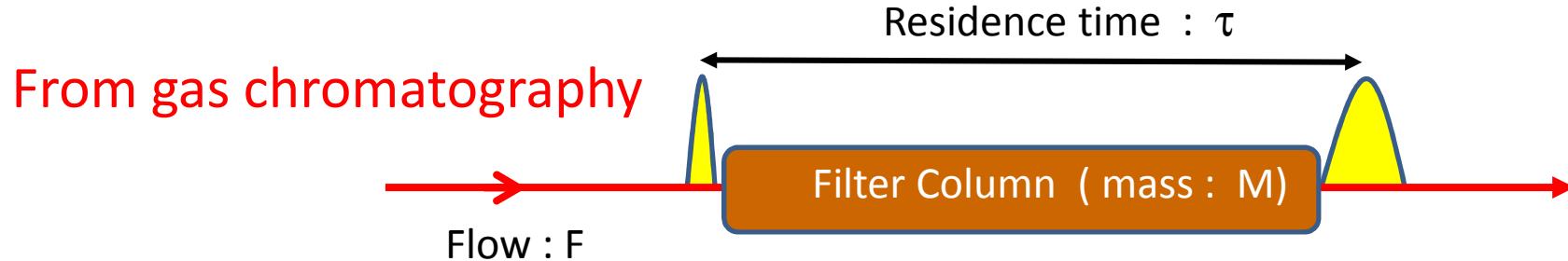
Radon in filter material by  $\gamma$ -Ge spectrometry



Radon  
concentration

$$K \left[ \text{m}^3/\text{kg} \right] = \frac{\text{Rn activity in the trap} [\text{Bq}/\text{kg}]}{\text{Rn activity in the gas} [\text{Bq}/\text{m}^3]}$$

# Residence time v. s. adsorption capacity



$$\tau = \frac{K_{\text{chr}} \cdot M}{F}$$

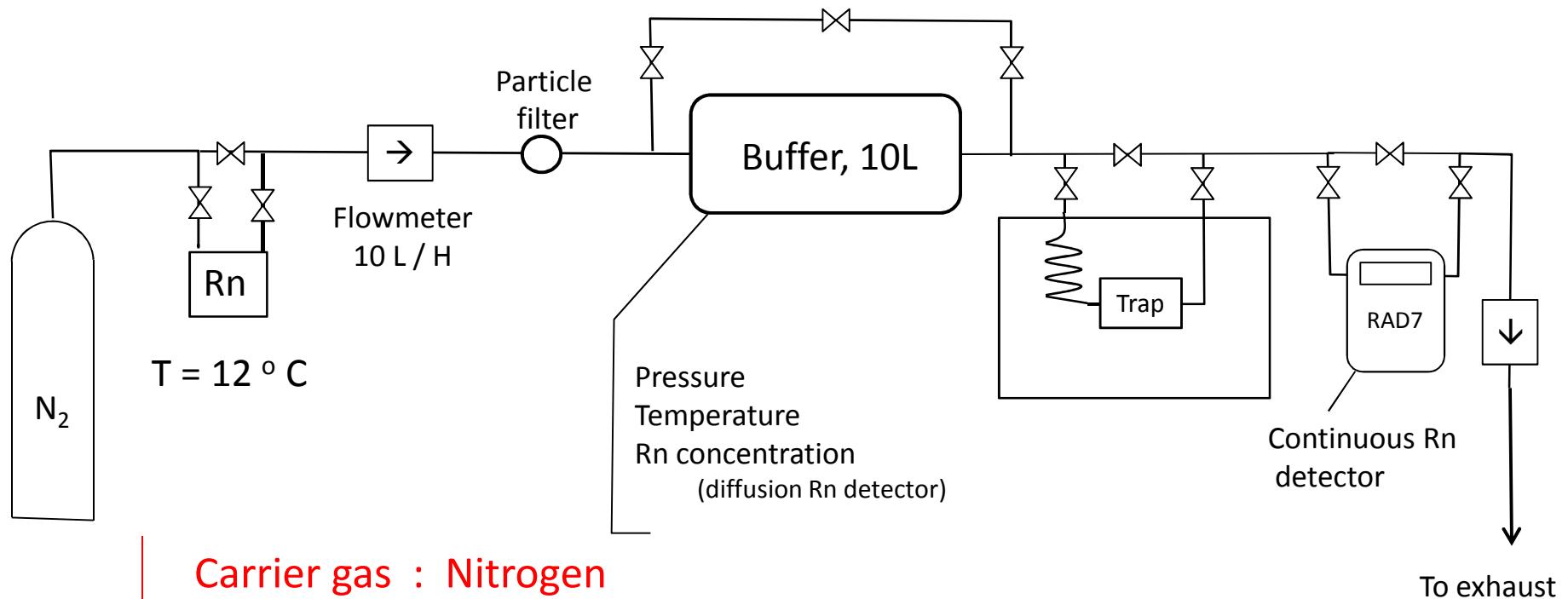
Mass

Flow

If  $K$  is big enough  $\Rightarrow \tau \gg T_{1/2}(\text{Rn})$   
the Rn concentration after the radon trap is negligible

# Experimental setup

## Dynamic Rn adsorption



Carrier gas : Nitrogen

Flow : 10 L / H

Rn concentration :  $\sim 900 \text{ Bq} / \text{m}^3$

Trap temperature :  $+20^\circ \text{C}$  to  $-80^\circ \text{C}$

Pressure : 1 bar

To exhaust

# Measured materials

T = 20 °C, -30 °C, -50 °C, -80 °C
P = 1 bar
Gas = Nitrogen, He

- Classical activated carbon : very wide pore size distribution
- Synthetic carbon : Carboact “popular” adsorbent in Low Radioactive Experiments
- Carbon molecular sieve : well defined pore size
- Metal Organic Framework : very large surface area
- Molecular Cages : well defined structure
- Zeolites : well defined structure; not low background
- Aerogel : large surface areas

# Results Active charcoal in N2

Echantillons	température C		K factor(m3/Kg)	erreur	K factor(m3/Kg)	erreur	K factor(m3/Kg)	erreur
	20	-30						
K48 SPECIAL	12,5	1,8	92,4	3,5	347,9	10,3		
K48	10,0	1,6	61,4	2,8	271,5	12,0		
ZORFLEX FM100	13,4	3,3	57,9	3,3	266,3	7,7		
NUCLEARCARB 208C 5KI3	6,9	1,3	43,3	2,5	209,5	7,0		
K610	6,2	1,3	22,1	2,6	170,2	6,0		
NUCLEARCARB 208C 5TEDA	3,9	1,2	29,9	2,1	97,5	4,3		
ENVIRONCARB 207C	2,2	1,0	12,1	1,7	49,1	3,3		

# Results

## Carbon Molecular Sieve, CARBOACT MOF in N<sub>2</sub>

Echantillons	température C		-30		-45	
	20	erreur	K factor(m <sup>3</sup> /Kg)	erreur	K factor(m <sup>3</sup> /Kg)	erreur
CARBOSEIVE SIII	10,0	6,1	168,4	9,5	728,5	32,9
CARBOSIEVE G			81	6,5		
CARBOXEN 1000	10,8	8,4	80,8	6,7	645,3	27,9
CARBOXEN 1012			150	7,6		
CARBOXEN 1020			82	6,1		
CARBOXEN 1018			136	8,2		
CARBOXEN 569	2,2	6,3	9,7	3,9	99,8	5,7
CARBOACT	20,5	2,9	131,9	4,1	425,5	11,4
MOF Basolite C300	8,7	4,8	215,2	10,3	409,2	10,6

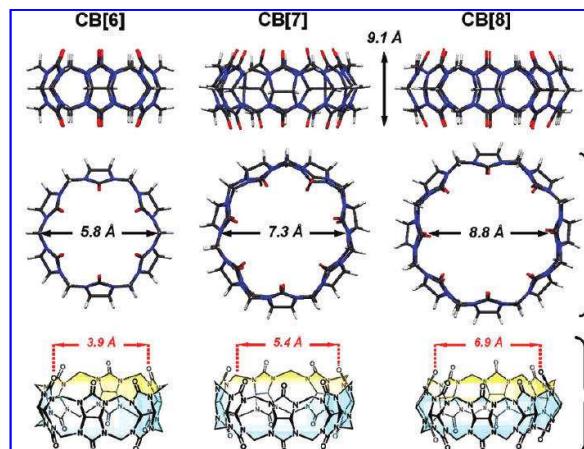
Big surface area. Very fine powder

Very low background

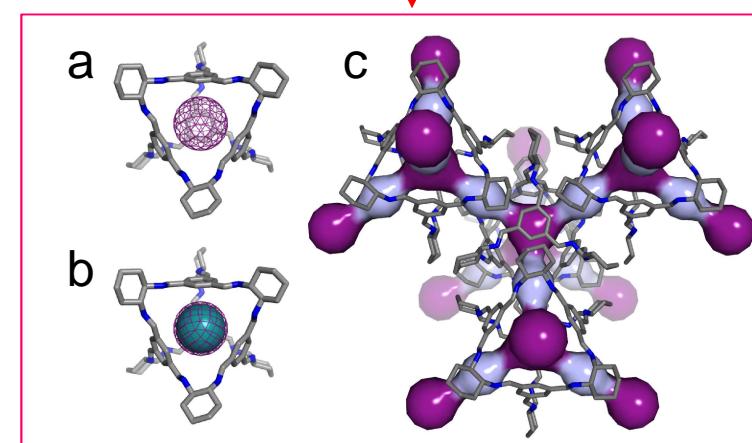
Well defined porosity

# Results molecular cages in N<sub>2</sub>

Echantillons	température C		erreurs	K factor(m <sup>3</sup> /Kg)	erreurs	K factor(m <sup>3</sup> /Kg)	erreurs
	20	-30					
CB[6]	1,4	7,4		1,1	3,8	19,9	9,9
CB[7]	5,0	7,1				10,3	10,1
CB[8]	8,1	9,2				5,2	6,2
PYR C7	2,5	8,7				4,6	4,7
REC10	4,6	9,9				2,6	5,5
C3 cage	6	7,1	25	3,2	89,9	4,2	



Curcubiturils



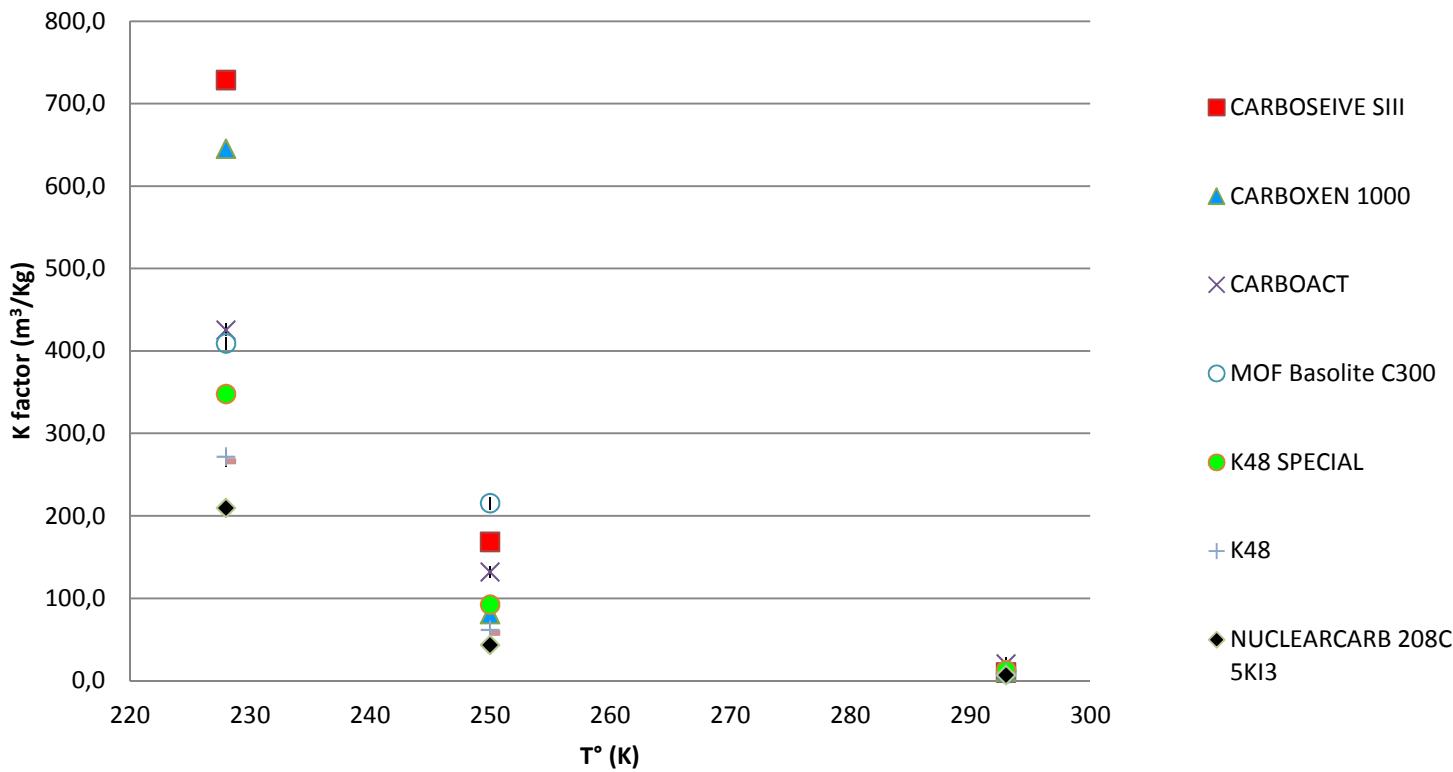
Porous organic cages CC3

# Results Carbon aerogel in N2

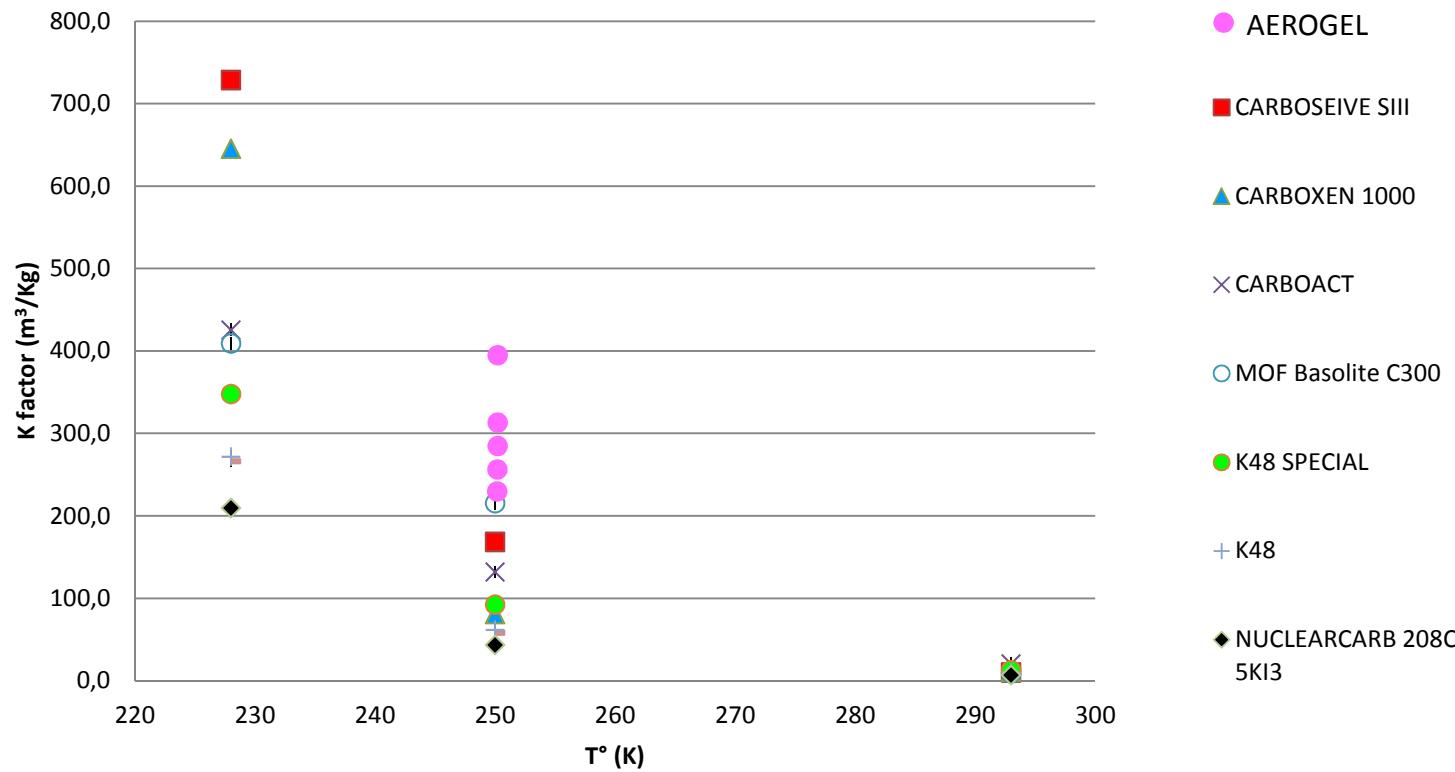
Echantillons	température C		K factor(m3/Kg)	erreur
	20	-30		
AEROGEL D			298	11
AEROGEL J			250	10
AEROGEL K			220	10
AEROGEL K11			317	13
AEROGEL J18			380	13

Very promising adsorbent

## Some K factor in fonction of temperature in N2



### Some K factor in fonction of temperature in N2



# Results in He

Echantillons	-30	-50	-80
	K factor(m3/Kg)	K factor(m3/Kg)	K factor(m3/Kg)
G2X4 (XMASS Charcoals)		2102+-60	6800+-240
CARBOXEN 1012		5672+-220	8000+-350
K48 special		2553+-85	
K48		2200+-60	
CARBOACT		7865+-280	
CARBOSIEVE III		9900+-370	
Aerogel D	1840+-64	4450+-160	
Aerogel J		5400 +- 230	
Aerogel K		6900 +- 250	
Aerogel K11		8300 +- 320	
Aerogel J18			

Very low competition between Rn and He

Very long measurements : ~ 10 days @ - 50 °C, 10 L /h and 0.3 gr

# Randon capture v.s. porosity

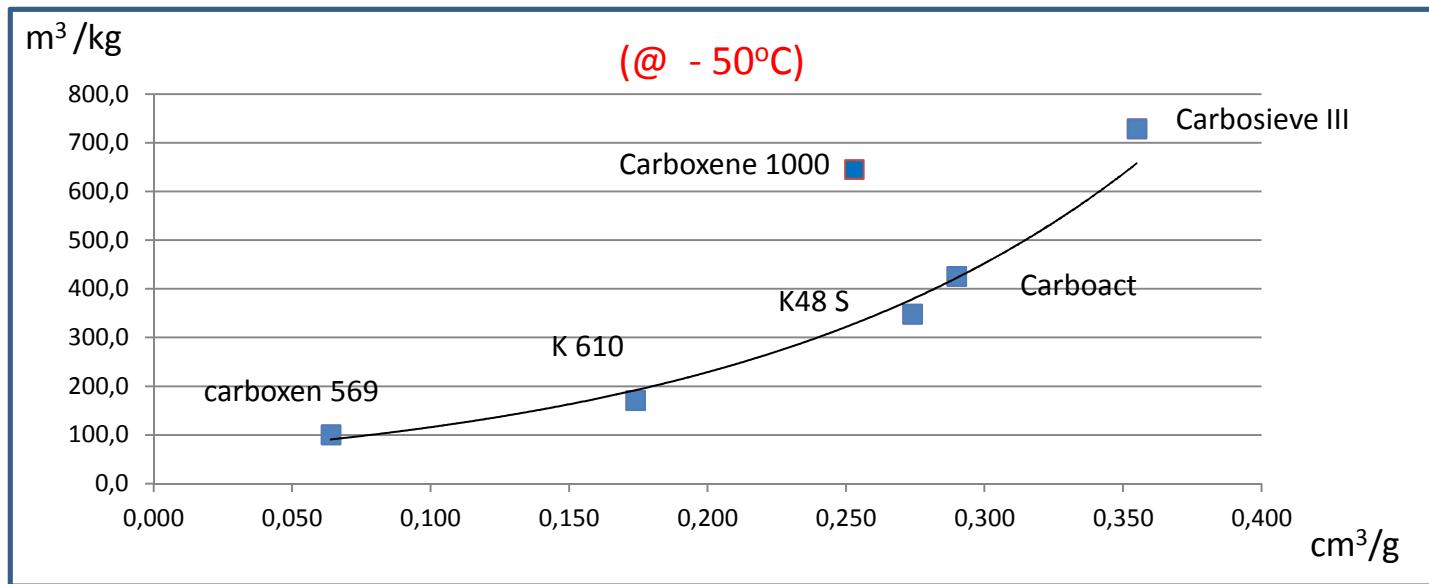
Echantillons	$A_{BET}$	Volume total	Volume microporeux total			Volume ultramicro	% ultra	Volume supermicro	$A_{ext}$
			t-plot	$\alpha_s$ -plot	DR				
			$m^2 \cdot g^{-1}$	$cm^3 \cdot g^{-1}$	$cm^3 \cdot g^{-1}$				
K610	940	0,381	0,370	0,410	0,348	0,174	42	0,236	40
Carboxen 569	290	0,484	0,080	0,064	0,117	0,064	100	0,000	164
Pleisch(CH)	1340	0,613	0,553	0,563	0,506	0,291	52	0,272	31
K48 special	1268	0,512	0,505	0,507	0,520	0,274	54	0,233	5
Carboact	1182	0,534	0,470	0,462	0,476	0,290	63	0,172	26
Carboxen 1000	931	0,842	0,357	0,359	0,366	0,253	70	0,106	20
Carbosieve SIII	1362	0,565	0,510	0,510	0,535	0,355	70	0,155	8

Ultramicropore :

diamètre < 1,062 nm

# Adsorption v. s. microscopic properties

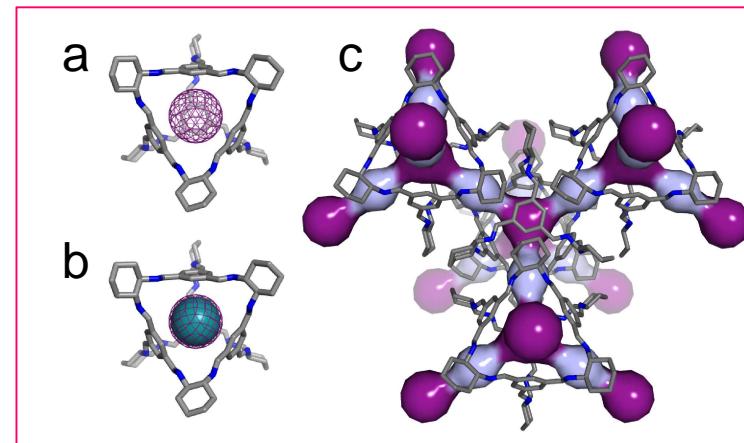
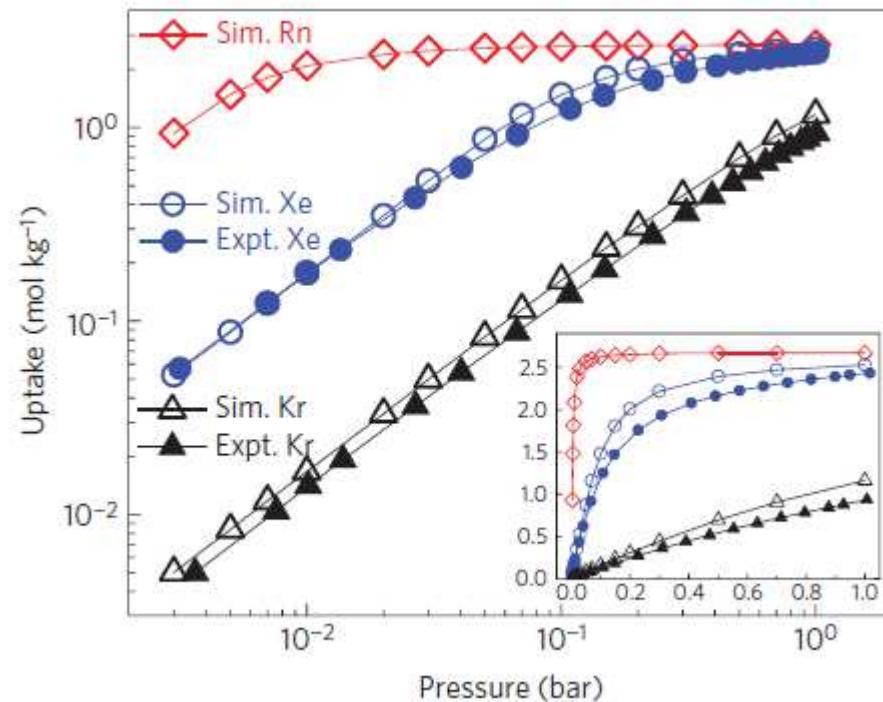
Adsorption ( m<sup>3</sup> /kg) v.s volume of ultramicropores ( < 1.62 nm)



*Very good correlation*

⇒ Modelization of radon adsorption

# Modelization is possible in “symmetric” carbon cages



# Self emanation

## Radioactivity of some active charcoals

Charcoal sample	Activity (Bq/kg)			
	$^{137}\text{Cs}$	$^{40}\text{K}$	$^{228}\text{Th}$	$^{226}\text{Ra}$
K48	$0.23 \pm 0.07$	$306 \pm 8$	$\leq 0.11$	$\leq 0.25$
K48 spe	$0.22 \pm 0.07$	$19 \pm 2$	$0.36 \pm 0.13$	$0.28 \pm 0.18$
EnviroCarb 207c 8x16 US	$1.1 \pm 0.1$	$256 \pm 8$	$0.45 \pm 0.11$	$0.23 \pm 0.17$
KG10	$\leq 0.22$	$\leq 3.3$	$14 \pm 1$	$23 \pm 1$
NuclearCarb 208c 5ki3	$\leq 0.13$	$475 \pm 12$	$\leq 0.11$	$\leq 1.7$
NuclearCarb 208c 5TEDA	$\leq 0.23$	$335 \pm 12$	$0.64 \pm 0.16$	$\leq 0.30$

Radon emanation from the trap it self

- *Very pure adsorbent ( synthetic materials )*
- *Mass of adsorbent as low as possible*

→ *Self adsorption can help*

# Conclusion

- Radioactivity from noble gases is an important background source in many low energy and low count rate experiments.
- Adsorption in microporous materials is possible but depends on porosity characteristics and carrier gas competition.